

1 **Amidohydrolase Process, a cascade chemoenzymatic process for**
2 **multisubstrate conversion to optically pure L-amino acids by dynamic kinetic**
3 **resolution**

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27 **ABSTRACT**

28 A bienzymatic system containing a *N*-succinylamino acid racemase from *Geobacillus*
29 *kaustophilus* CECT4264 (GkNSAAR) and of L-*N*-carbamoylase from *Geobacillus*
30 *stearothermophilus* CECT43 (BsLcar) has been developed. This biocatalyst was able to
31 produced optically pure natural and non-natural L-amino acids from racemic mixtures
32 of *N*-acetyl, *N*-formyl- and *N*-carbamoyl-amino acids by dynamic kinetic resolution,
33 showing the fastest conversion on the *N*-formyl-amino acids followed by *N*-carbamoyl
34 and *N*-acetyl ones. Metal ion cobalt was essential for the activity of the biocatalyst. Co^{2+}
35 was added during protein induction or preincubated with the recombinant enzymes
36 before reaction or directly added into this, and the system was optimally active when
37 Co^{2+} was added directly to the reaction. Optimum reaction conditions for the biocatalyst
38 were pH 8 and 45 and 65°C for *N*-formyl- and *N*-carbamoyl-amino acids, respectively.
39 The bienzymatic system was equally efficient to convert aromatic and aliphatic
40 substituents but always faster *N*-formyl than *N*-carbamoyl-amino acids. This new
41 Amidohydrolase Process enables the natural and unnatural L-amino acids production
42 from broad substrate spectrum.

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52 INTRODUCTION

53 Optically pure natural and non-natural L-amino acids are of considerable
54 economic importance because of the broad spectrum of their industrial applications. The
55 former, proteinogenic amino acids are building block of life, used in human nutrition
56 and health or as additives, flavour enhancers and sweeteners (5). Additionally, non-
57 natural L-amino acids are in increasing demand as valuable intermediates in the
58 pharmaceutical industry. By way of example, L-homophenylalanine is a precursor for
59 the preparation of angiotensin-converting enzyme (ACE) and rennin inhibitors, such as
60 enalapril, lisinopril, quinapril, ramipril,trandolapril and benazepril, among others (10).
61 L- α -aminobutyric acid (L-ABA) is an intermediate of ophthalmate, a sensitive indicator
62 of hepatic glutathione (GSH) depletion, and designed as new biomarker for oxidative
63 stress (18).

64
65 Biocatalytic methods based on chemo-enzymatic processes have been described
66 for optically pure amino acid production. Some of these methods are the hydantoinase
67 (6), amidase (2) and acylase (14) processes. The “Hydantoinase Process” is based on the
68 dynamic kinetic resolution of D,L-5-monosubstituted hydantoins using an inexpensive
69 and environmental friendly enzymatic method (1). The chirality of the amino acid
70 obtained depends on the stereospecificity of the last enzyme in the reaction cascade (*N*-
71 carbamoyl-L-amino-acid amidohydrolases, also known as L-*N*-carbamoylases) (13). In
72 the “Acylase process” a *N*-acylamino acid racemase (NAAAR) together with a L-
73 aminoacylase can produce a final yield of 99% optically pure amino acid in one step
74 from racemic mixtures of *N*-acylamino acids, by enzymatic racemization of the non-
75 hydrolysed *N*-acetyl-L-amino acid (21).

76 Our group has recently demonstrated the substrate promiscuity of a recombinant
77 *N*-succinylamino acid racemase from *Geobacillus kaustophilus* CECT4264
78 (GkNSAAR) (15) and of L-*N*-carbamoylase from *Geobacillus stearothermophilus*
79 CECT43 (BsLcar) (16). Both enzymes allowed the racemization or hydrolysis of *N*-
80 acetyl-, *N*-formyl- and *N*-carbamoyl-amino acids. The aim of this work is to develop a
81 biocatalyst joining both enzymes as a bienzymatic system for natural and non-natural
82 optically pure L-amino acids production. This Amidohydrolase Process will be able to
83 convert racemic mixtures of *N*-acetyl-, *N*-carbamoyl- and *N*-formyl-amino acids into L-
84 amino acids, with 100% of yield, by dynamic kinetic resolution.

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101 MATERIALS AND METHODS

102 General protocols and reagents.

103 Standard methods were used for the cloning and expression of the different
104 genes (3,17). Restriction enzymes, T4 DNA ligase and the thermostable *Pwo*
105 polymerase together with primers for PCR were purchased from Roche Diagnostic S.L.
106 (Barcelona, Spain). Racemic mixtures and optically pure D- and L-amino acids were
107 purchased from Sigma Aldrich Quimica S.A. (Madrid, Spain). *N*-acetyl D- and L-
108 methionine were purchased from Sigma-Aldrich (Madrid, Spain). The *N*-carbamoyl-
109 and *N*-formyl-amino acids were synthesized according to previous works (4,9).

110

111 Plasmids and culture conditions.

112 Two recombinant *Escherichia coli* BL21 strains were grown in Luria-Bertani
113 medium (LB) (1% tryptone, 0.5% yeast extract, 0.5% NaCl, pH 7.2) as previously
114 described (15,11). One harboured pJAVI80 containing L-*N*-carbamoylase gene from
115 *Geobacillus stearothermophilus* CECT43 (*Bslcar*) and the other harboured pJPD25
116 containing *N*-succinylamino acid racemase gene (*nsaar*) from *Geobacillus kaustophilus*
117 CECT4264 (*Gknsaar*). Both genes were taken from the above mentioned plasmids and
118 cloned in the rhamnose-inducible expression with His-tag pJOE4036.1 (20);
119 Altenbuchner, pers. communication), to increase the overexpression of the genes in *E.*
120 *coli* BL21 strains (19). The development of the plasmid pJAVI80rha is described in
121 (12).

122 The pJPD25rha construction was made by PCR amplification of *Gknsaar* gene
123 (1128 bp; Genbank accession no. EU427322) from the recombinant plasmid pJPD25
124 that was used as template (16). The PCR primers were 5′-
125 AGAAAGGGGAGAGCTCATGGCGATCAACA-3′ (the *Sac*I site in italics) and 5′-

126 GGATCCTGCCGTCGCCGTACGATGAAACA-3' (the *Bam*HI site in italics).
127 Amplifications were performed in a Applied Biosystems thermal cycler 2720
128 programmed as follows: initial denaturation at 94°C for 5 min; 30 sec at 94°C for
129 denaturing, 30 sec at 57°C for annealing, 1 min at 72°C for synthesis, repeated 35
130 cycles; and a final extension step of 5 min at 72°C. The PCR products were purified
131 from agarose gel using E.Z.N.A. Gel Extraction Kit (Omega Bio-Tek, Inc., USA),
132 treated with the corresponding enzymes and then ligated into pJOE4036.1 which was
133 cut with the same enzymes to create the plasmid pJPD25rha.

134 After cloning, the plasmid was transferred to *E. coli* DH5 α to verify the presence
135 of the insert. The sequence was analyzed at least twice using standard T3 and T7
136 primers. Sequencing analysis was carried out using the dye dideoxy nucleotide
137 sequencing method in an ABI 377 DNA Sequencer (Applied Biosystems).

138

139 **Expression of *Bslcar* and *Gknsaar* genes.**

140 The transformants in BL21 strain (BL21pJAVI80rha and BL21pJPD25rha) were
141 grown in LB medium supplemented with 100 $\mu\text{g ml}^{-1}$ of ampicillin. The expression
142 protocol was the same both transformants. A single colony was transferred into 10 ml of
143 LB medium with ampicillin at the above-mentioned concentration in a 100 ml flask.
144 This culture was incubated overnight at 37°C with shaking. In a 2 l flask 500 ml of LB
145 with the appropriate concentration of ampicillin was inoculated with 5 ml of the
146 overnight culture. After 2 h of incubation at 37°C with vigorous shaking, the OD₆₀₀ of
147 the resulting culture was 0.3-0.5. For expression induction of the *lcar* and *nsaar* genes,
148 L-rhamnose (Prolabo, VWR) was added to a final concentration of 0.2 % (w/v) and the
149 culture was incubated at 32°C for an additional 6 hours. The cells were collected by
150 centrifugation (Beckman JA2-21, 7,000 g, 4°C, 10 min) and stored at -20°C. The

151 freezed pellet was washed twice and resuspended in 50 ml wash buffer (300 mM NaCl,
152 20 mM imidazole, 50 mM sodium phosphate; pH 7.0). The cell walls were disrupted in
153 ice by sonication using a UP 200 S Ultrasonic Processor (Dr. Hielscher GmbH,
154 Germany) for 6 periods of 60 s, pulse mode 0.5 and sonic power 60%. The pellet was
155 precipitated by centrifugation (Beckman JA2-21, 10,000 g, 4°C, 20 min) and discarded.
156 The supernatant was applied to a column with TALON™ metal affinity resin
157 (CLONTECH Laboratories, Inc., Nucliber, Madrid, Spain) and then washed three or
158 four times with wash buffer. After washing, BsLcar and GkNSAAR were eluted with
159 elution buffer (100 mM NaCl, 150 mM imidazole, 2 mM Tris, pH 8.0). The purified
160 enzymes were dialysed against 0.1 M borate/HCl pH 8.0 and stored at -20°C until use.

161

162 **Conversion assay.**

163 Standard enzymatic reaction was carried out with the purified BsLcar and
164 GkNSAAR enzymes (at a final concentration of 3.1 μM and 8.1 μM, respectively) in
165 presence of CoCl₂ (final concentration of 1 mM) together with *N*-derivate of D,L-
166 methionine as substrate (15 mM) dissolved in 100 mM borate/HCl (pH 8.0) in 390 μl
167 reaction volume. The reaction mixture was incubated at 65°C and 60 min for *N*-
168 carbamoyl-D,L-methionine conversion and 15 min at 45°C for *N*-formyl-D,L-
169 methionine one. For *N*-acetyl-D,L-methionine conversion final concentration of BsLcar
170 and GkNSAAR enzymes was 35.64 μM and 73.49 μM, respectively, with a reaction
171 time of 240 min at 65°C. The reactions were stopped by addition of 10 times the
172 reaction volume of 1% H₃PO₄.

173 After centrifuging, the resulting supernatants were analysed by high
174 performance liquid chromatography (HPLC). The HPLC system (LC2000Plus HPLC
175 System, Jasco, Madrid, Spain) equipped with a Luna C₁₈ column (4.6 × 250 mm,

176 Phenomenex) was used to detect *N*-acetyl, *N*-formyl and *N*-carbamoyl-D,L-methionine
177 and L-methionine. The mobile phase was methanol/phosphoric acid (20 mM, pH 3.2)
178 (vol/vol, 20:80), pumped at a flow rate of 0.80 ml min⁻¹ and measured at 200 nm.

179 Substrate specificity studies were performed with each different *N*-formyl and
180 *N*-carbamoyl-amino acid dissolved in 100 mM borate/HCl (pH 8.0) together with the
181 purified enzyme at the same concentration described above in presence of 1 mM CoCl₂.
182 Reactions were carried out at 45 °C and 65°C, and stopped by addition of 1% H₃PO₄.
183 The mobile phase of the different substrates and their corresponding L-amino acids was
184 methanol-phosphoric acid (20 mM, pH 3.2) (5:95 to 50:50 vol/vol, depending on the
185 compound), pumped at a flow rate of 0.50 ml min⁻¹. Compounds were detected with a
186 UV detector at a wavelength of 200 nm.

187

188 **System characterization.**

189 Optimal temperature was evaluated from 30 to 80 °C in 100 mM borate/HCl (pH
190 8.0). The thermal stability of the cascade enzymatic process was measured after 0, 2, 4,
191 6, 8, 10 and 24 hours of preincubation at temperatures from 40 to 70 °C in 100 mM
192 sodium borate/HCl buffer pH 8. Studies of pH were assayed in several buffers at pH 5.5
193 to 10.5 (sodium citrate, sodium cacodylate, borate/HCl and borate/NaOH) at a
194 concentration of 100 mM. Enzyme assays, for optimal temperature and pH studies, were
195 then carried out at 45 °C for 30 min with *N*-formyl-D,L-methionine and 65°C for 60 min
196 with *N*-carbamoyl-D,L-methionine.

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201 RESULTS AND DISCUSSION

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203 Multisubstrate hydrolysis

204 Recombinant BsLcar has demonstrated to hydrolyse *N*-acetyl and *N*-formyl-
205 amino acids in addition to *N*-carbamoyl-amino acids (16). Additionally, GkNSAAR has
206 shown the ability to racemize different *N*-acetyl and *N*-carbamoyl-amino acids (15).
207 Evidenced this substrate promiscuity of both enzymes, BsLcar and GkNSAAR were
208 combined to transform *N*-acetyl, *N*-formyl- and *N*-carbamoyl-amino acids into optically
209 pure L-amino acids. The bienzymatic system was able to hydrolyse all three racemic
210 substates into L-methionine, showing the fastest conversion on the *N*-formyl-amino acid
211 followed by *N*-carbamoyl and *N*-acetyl ones (Fig. 1), for this we have named it as
212 “Amidohydrolase Process”. These results are in accordance with those obtained for
213 BsLcar, where the highest conversion was for *N*-formyl-amino acids followed by *N*-
214 carbamoyl- and *N*-acetyl-amino acids (16). Previous studies with GkNSAAR
215 demonstrated that catalytic efficiency (k_{cat}/K_m) to racemize both isomers of *N*-acetyl-
216 and *N*-carbamoyl-methionine were very similar (15), and there is no data about
217 racemization of *N*-formyl-amino acids with GkNSAAR. From the present studies with
218 de bienzymatic system and those with BsLcar and GkNSAAR separately, we can
219 assume that BsLcar is the responsible that *N*-formyl amino acids are fastest hydrolysed
220 compared with the *N*-carbamoyl- and *N*-acetyl- ones. At last, when *N*-succinyl-amino
221 acids, the natural substrates of GkNSAAR, were used as substrates for BsLcar we did
222 not detect any activity (data not shown).

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226 **Effect of enzyme ratios in the bienzymatic system**

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228 Enzyme ratio plays a critical role in driving the overall reaction. Optimize the
229 right proportion of each enzyme allows to reduce both time reaction and protein
230 consumption. BsLcar has shown higher catalytic efficiency for the hydrolysis of these
231 types of substrates than GkNSAAR to racemize them (15,16). Five different
232 BsLcar/GkNSAAR ratios, with constant presence of BsLcar and always increasing the
233 GkNSAAR proportion in the mixture (1:1, 1:3, 1:6, 1:12 and 1:18), were assayed to
234 achieve maximum conversion efficiencies for L-methionine from *N*-formyl-D,L-
235 methionine (Figure 2). When the proportion of both enzymes was the same (ratio 1:1),
236 the conversion was only 50% after 350 min of reaction. After increased 6, 12 and 18
237 times GkNSAAR proportion respect BsLcar, conversion efficiencies approached nearly
238 100%. In order to reduce GkNSAAR consumption 1:6 ratio was selected as the best for
239 biocatalytic transformation (Fig. 2).

240

241 **Cobalt effect in the bienzymatic system**

242 BsLcar and GkNSAAR have been described as metalloenzymes and for both
243 enzymes Co^{++} as the best cofactor (15,16). For GkNSAAR it is not necessary a
244 preincubation with the metal ion for hours and the Co^{++} is adding directly to the reaction
245 as a component (15). However, our previous studies for BsLcar were made with
246 preincubation with Co^{++} at 4°C (16). In order to balance the way to obtain the active
247 protein by metal ion, two strategies were developed: a) compare the BsLcar activity
248 after preincubation with Co^{++} after adding the metal ion directly in the reaction, in order
249 to avoid the preincubation, and b) include Co^{++} in the grow medium to obtain
250 recombinant enzymes including active avoiding to add the metal ion in the reaction.

251 To evaluate the first strategy, BsLcar was incubated at 4°C for 60 min with 1
252 mM Co⁺⁺ to enhance the activity. However, there was no activity difference between
253 preincubated BsLcar and when the metal ion was added directly to the reaction (data not
254 shown). Thus, to activate the enzymes is enough adding Co⁺⁺ in the reaction directly,
255 avoiding time consuming in enzyme preincubation.

256 The second strategy tried to avoid adding the cobalt in the reaction by including
257 this in the induction step. For this, BL21 pJAVI80rha and BL21 pJPD25rha were
258 induced as described in materials and methods, but including Cl₂Co 0.2 mM at the end
259 concentration. BsLcar activity was the same for both BsLcar overexpressed in a medium
260 supplemented with Co⁺⁺ and that one induced without metal ion but added directly to
261 the reaction (Fig. 3A). In opposite, GkNSAAR was not active at all when the enzyme
262 was overexpressed in a medium supplemented with Co⁺⁺ (Fig. 3B), restoring the activity
263 after adding directly Cl₂Co 1mM to the reaction mixture. Additionally, two effects were
264 detected when Co⁺⁺ was included in the cells grow medium: a) a toxic effect in bacterial
265 cells decreasing the number recombinant cells produced during the induction,
266 consequently the purified protein yield drastically dropped, and b) substantial
267 insolubility of the recombinant enzymes produced by cells that accumulate the Co⁺⁺
268 during the grow and induction. Thus, BsLcar could be concentrate up to 20 mg/ml if the
269 cells were grown without Co⁺⁺ and 7.7 mg/ml in presence of the metal ion. Similar
270 phenomenon was detected for GkNSAAR, where the solubility down from 17 to 9.5
271 mg/ml, without and with metal ion, respectively. All these studies ended in directly
272 addition of Co⁺⁺ in the reaction mixture.

273 For determinate the optimum Co⁺⁺ concentration in the reaction, Cl₂Co from 0 to
274 6mM was added to the reaction (Fig. 4). In absence of cobalt the bienzymatic system
275 only transformed 50% of the substrate in optically pure L-amino acid. This result agrees

276 with those that demonstrated BsLcar activity with no cobalt in the reaction (16), and in
277 the bienzymatic system this activity let the hydrolysis of the L-isomer of the racemic
278 formyl-methionine used as substrate. However, GkNSAAR was previously described as
279 inactive without cobalt in reaction (15), and thus in the bienzymatic system the enzyme
280 can not racemize the non-hydrolysed by BsLcar D-isomer. When the metal ion was
281 presented in the reaction the conversion was 100% in the same time (Fig. 4) with no
282 noticeable inhibition at higher cobalt concentrations (6 mM). Optimal conversion by
283 bienzymatic system was detected at 0.25 mM of Co²⁺, and from now this is metal ion
284 concentration used in standard reaction.

285

286 **pH and temperature effect in the bienzymatic system**

287 As we have described above the bienzymatic system transformed *N*-formyl, *N*-
288 carbamoyl- and *N*-acetyl-amino acids into optically pure L-amino acids, but those latter
289 very much slowly. For this reason the conversion reaction was optimized for the two
290 former. Thus, L-methionine production from *N*-formyl and *N*-carbamoyl-methionine
291 was evaluated at different pHs and temperatures. Optimal pH to obtain the maximum
292 conversion efficiency of the system for both substrates was 8 (Fig. 5). This pH value is
293 the same that obtained for GkNSAAR (15) and slightly higher than for BsLcar (16) with
294 pH 7.5. BsLcar showed 95% of activity at pH 8, but GkNSAAR activity decreased until
295 80% at pH 7.5 (15,16), confirming pH 8 as the optimal for the bienzymatic system. The
296 temperature activity profile of the bienzymatic system for the two different substrates
297 was evaluated at different temperatures (Fig. 6). Maximum conversion activity was
298 different for *N*-carbamoyl- and *N*-formyl-methionine with 65 and 45°C, respectively.

299 The thermal stability of the cascade enzymatic process was measured after 0, 2,
300 4, 6, 8, 10 and 24 hours of preincubation at temperatures from 40 to 70 °C in 100 mM

301 sodium borate/HCl buffer pH 8. The bienzymatic system showed 100% of activity after
302 24 hours of preincubation at 45°C, down until 70 and 60% after 24 hours at 50 and
303 60°C, respectively (Fig. 7).

304

305 **3.5. Substrate conversion to L-amino acid by the bienzymatic system**

306 After optimized the bienzymatic system conversion reaction from *N*-formyl and
307 *N*-carbamoyl-amino acid to optically pure L-amino acid, this was evaluated for different
308 substrates (Fig. 8). A previous work demonstrated the ability to produce L-
309 homophenylalanine from racemic mixtures of *N*-carbamoyl- D,L-homophenylalanine by
310 using a NSAAR from *Deinococcus radiodurans* and L-*N*-carbamoylase from *Bacillus*
311 *kaustophilus* in a recombinant *E. coli* whole cell system, but not other L-amino acids
312 (8). However, and to our knowledge, this is the first work to report a system able to
313 convert, not only racemic mixtures of *N*-carbamoyl-amino acids, but also *N*-formyl-
314 amino acids into optically pure L-amino acids. Following the results, the biocatalytic
315 process converted more efficiently *N*-formyl than *N*-carbamoyl-amino acids into natural
316 and unnatural L-amino acids (Fig. 8). The bienzymatic system was equally efficient to
317 convert aromatic and aliphatic substituents. The highest initial reaction rate has been for
318 the unique natural L-amino acid used as control in this work, L-methionine, with 0.6377
319 and 0.1581 U/mg protein from *N*-formyl and *N*-carbamoyl-methionine, respectively.
320 The substrates hydrolyzed most slowly were L-aminobutyric acid (L-ABA) and L-
321 phenylglycine, with aliphatic and aromatic substituents, respectively. However, this
322 enzymatic method using racemic substrates is more efficient than the previously
323 described for L-ABA production from optically pure L-threonine and L-aspartic acid in
324 a whole cell biotransformation using recombinant *E. coli* cells expressing cloned genes
325 for threonine deaminase, aromatic aminotransferase and acetolactate synthase (7).

326

327 The behaviour of the bienzymatic system in presence of high substrate
328 concentration in reaction is a crucial point of interest. For this reason, we have analyzed
329 the production of optically pure L-homophenylalanine from 100 mM *N*-formyl-
330 homophenylalanine (Fig. 9). In spite of the low solubility of the L-amino acid, upper
331 concentrations of 50 mM were not measurable, the total hydrolysis of the precursor
332 (Fig. 9) and the only presence of the L-amino acid in the powder at the end of reaction
333 by nuclear magnetic resonance (NMR) analysis (data no shown), have demonstrated the
334 100% conversion of the substrate. The total conversion was achieved in only 24 hours
335 using the same enzyme concentrations that at the small-scale without noticeable
336 inhibition effect for high substrate concentration.

337 This bienzymatic system has shown to be able to convert different racemic
338 mixtures of substrates (*N*-acetyl, *N*-formyl- and *N*-carbamoyl-amino acids) in optically
339 pure L-amino acids by dynamic kinetic resolution. This biocatalyst is a real alternative
340 for supply non-natural L-amino acids to the Pharmaceutical Industry.

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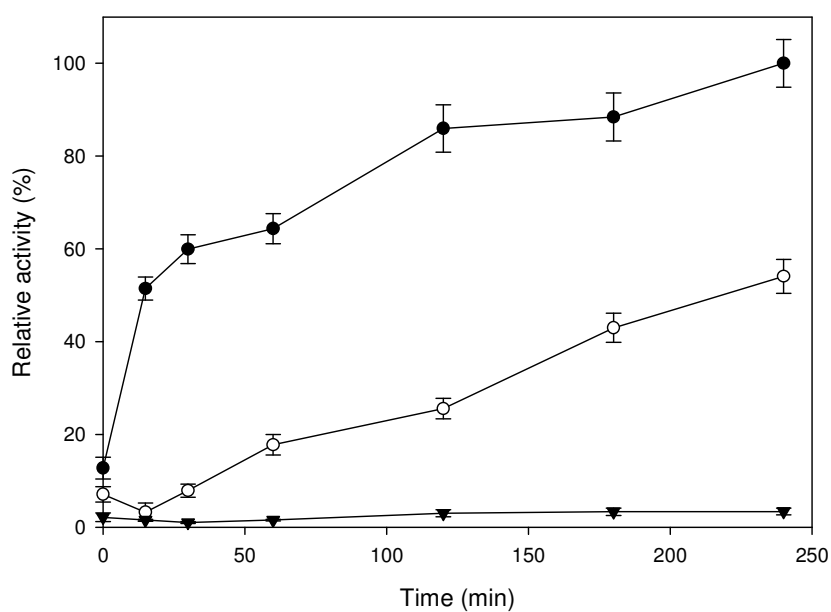
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437 Figure 1.- Optically pure L-methionine formation from *N*-formyl- (●), *N*-carbamoyl- (○)
438 and *N*-acetyl-methionine (▼) by using the Bienzymatic System formed by BsLcar and
439 GkNSAAR. Activity measures were performed using standard enzyme assay and in
440 triplicate (see Material and Methods).

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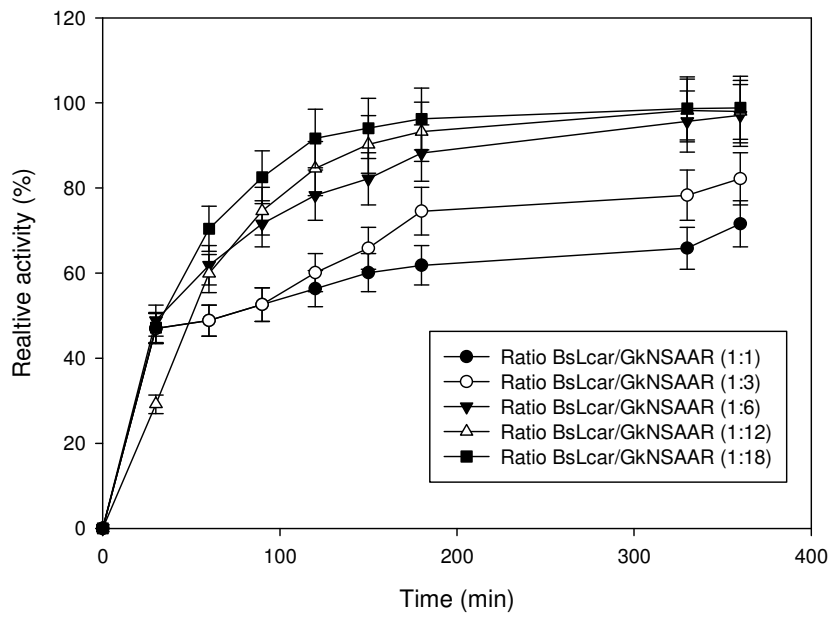


Figure 2.- Optically pure L-methionine formation from *N*-formyl-methionine by using the Bienzymatic System with different BsLcar and GkNAAAR ratios. Activity measures were performed using standard enzyme assay and in triplicate (see Material and Methods).

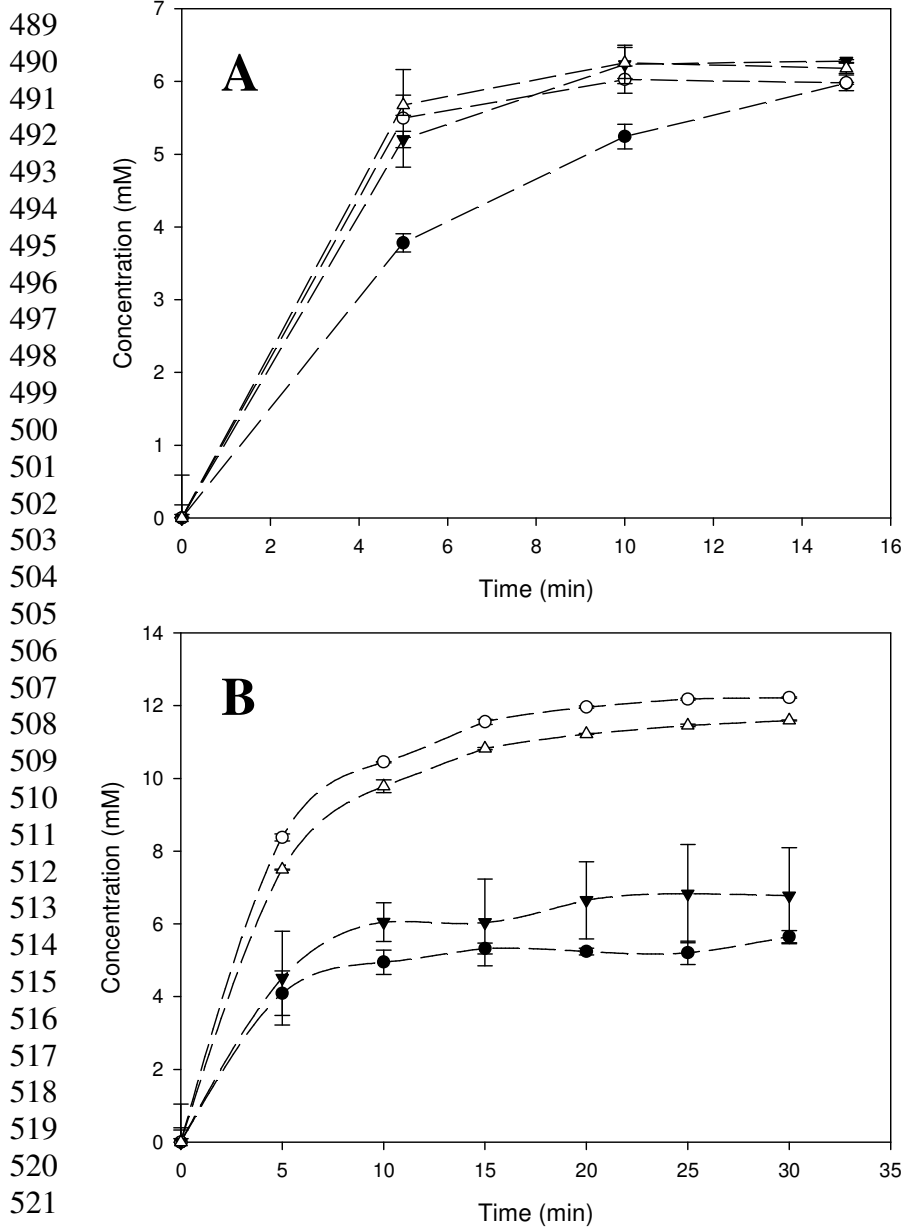
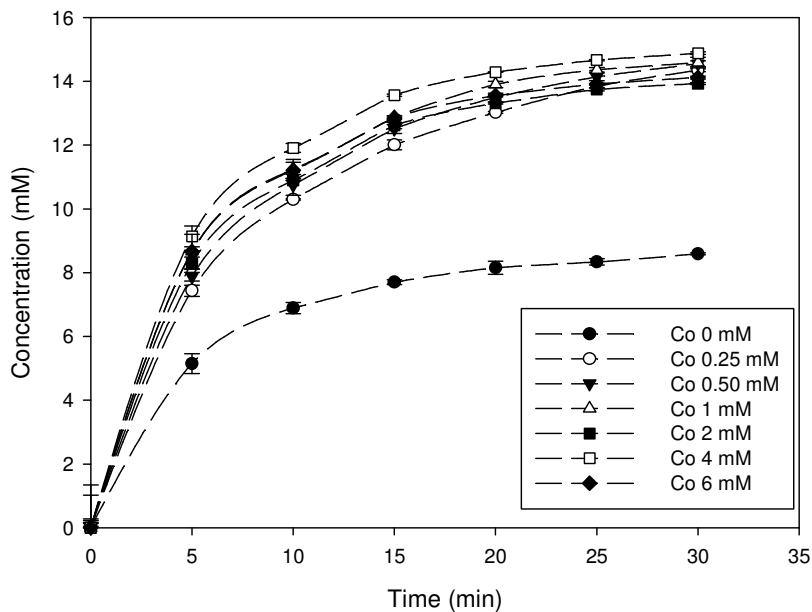


Figure 3.- Cobalt effect on BsLcar (A) and GkNSAAR (B). BsLcar activity was measured using *N*-formyl-D,L-methionine as substrate and the assays were performed in triplicate as described in (Pozo-Dengra, 2010). GkNSAAR activity was measured as accomplished reaction together BsLcar, using *N*-formyl-D,L-methionine as substrate and the assays were performed in triplicate as described in Material and Methods in presence of five times higher concentration of BsLcar. (●) Recombinant enzyme induced without Co⁺⁺ and reaction assay without Co⁺⁺, (○) recombinant enzyme induced without Co⁺⁺ and reaction assay with Co⁺⁺, (▼) recombinant enzyme induced with Co⁺⁺ and reaction assay without Co⁺⁺ and (△) recombinant enzyme induced with Co⁺⁺ and reaction assay with Co⁺⁺.



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555 **Figure 4.-** Cobalt effect on Bienzymatic System after adding several concentrations of

556 metal ion in the reaction mixture. Reactions were made using *N*-formyl-D,L-methionine

557 as substrate and the assays were performed in triplicate as described in Material and

558 Methods with a protein concentration of 13.81 μ M for GkNSAAR and 2.21 μ M for

559 BsLcar.

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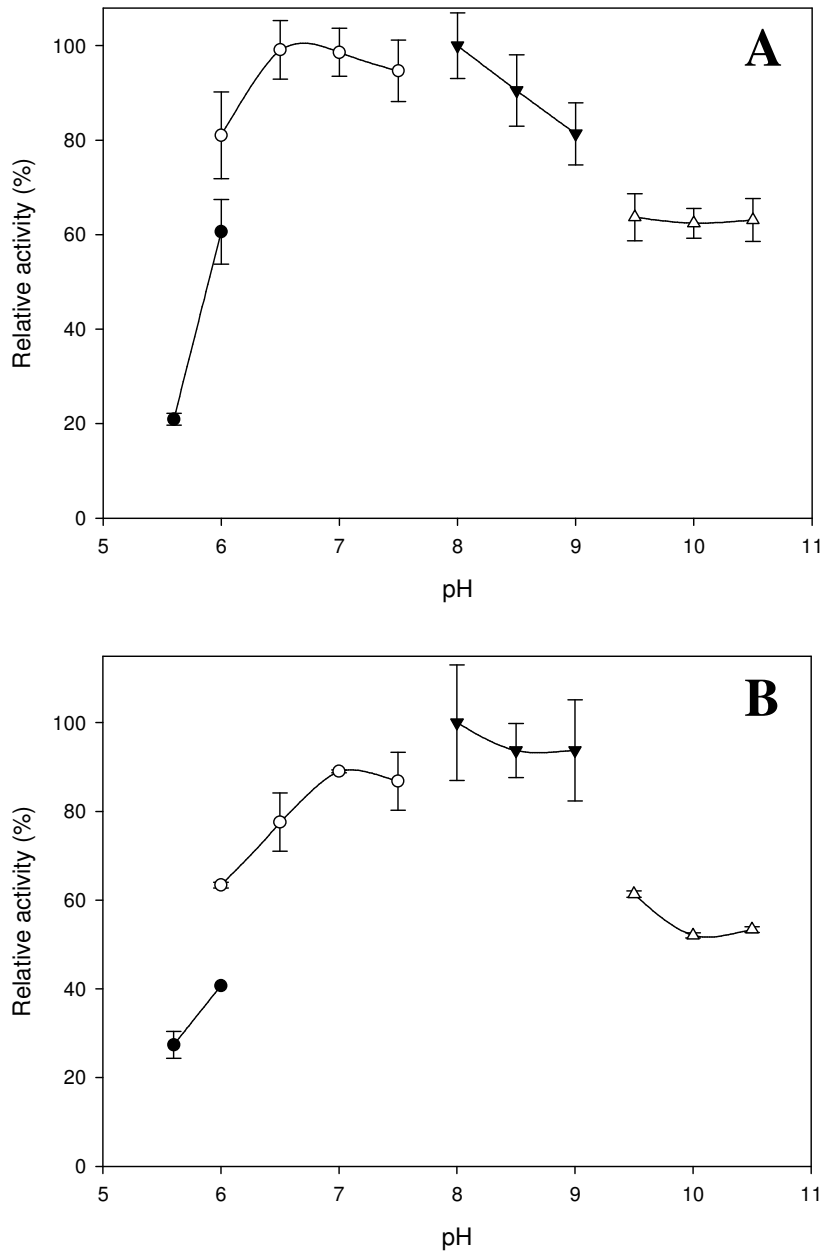


Figure 5. Effect of pH on *N*-carbamoyl- (A) and *N*-formyl-D,L-methionine (B) conversion into L-methionine. Studies of pH were assayed in several buffers at pH 5.5 to 10.5 (sodium citrate (●), sodium cacodylate (○), borate/HCl (▼) and borate/NaOH (△)) at a concentration of 100 mM. Enzyme assays were performed in triplicate as described in Material and Methods.

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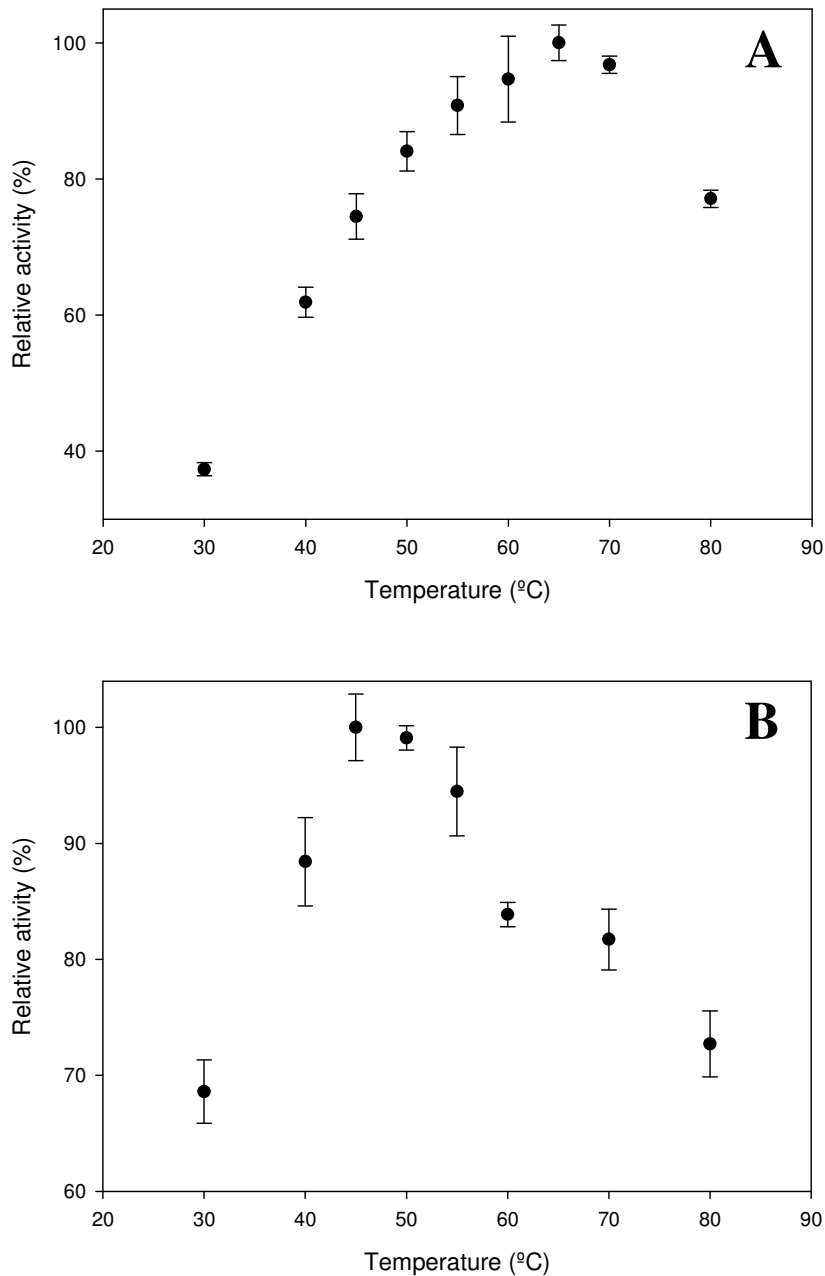


Figure 6. Effect of temperature on *N*-carbamoyl- (A) and *N*-formyl-D,L-methionine (B) conversion into L-methionine. Optimal temperature was evaluated from 30 to 80 °C in 100 mM borate/HCl (pH 8.0). Enzyme assays were performed in triplicate as described in Material and Methods.

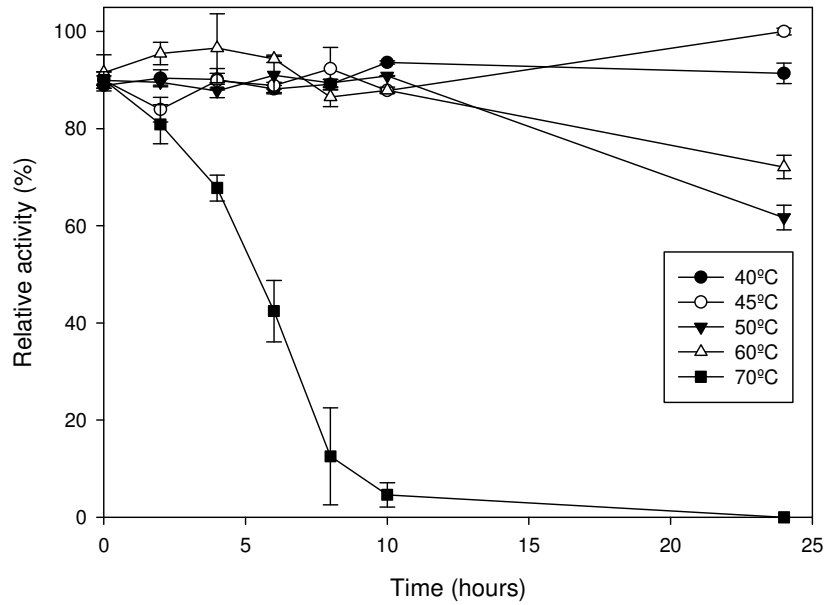
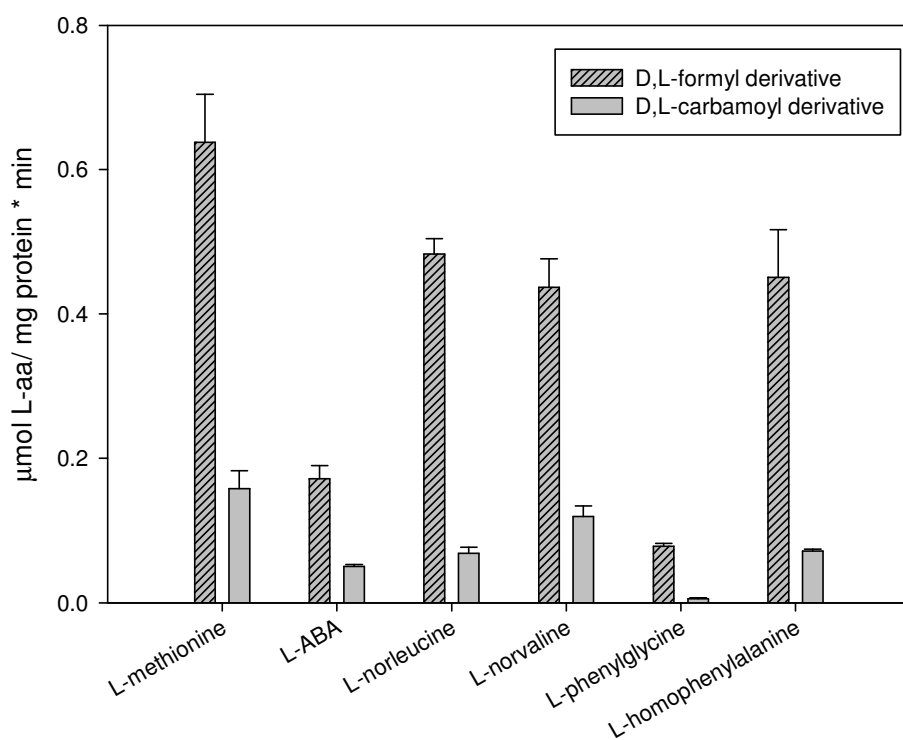
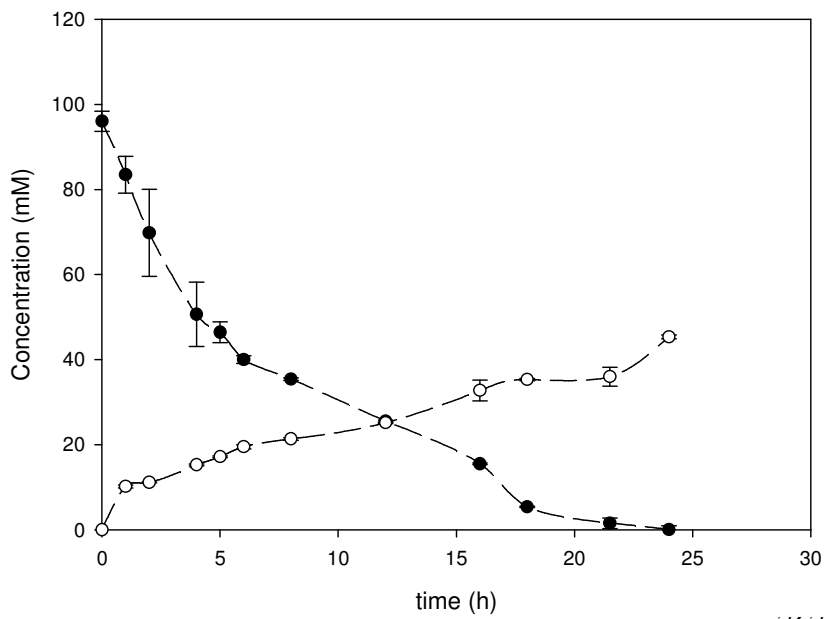


Figure 7. Thermal stability effect on L-methionine production from D,L-formyl methionine after different hours of preincubation at temperatures from 40 to 70 °C in 100 mM sodium borate/HCl buffer pH 8. Thermal stability was evaluated with standard assays performed in triplicate as described in Material and Methods.



725 **Figure 8.** Initial reaction rates for the production of different optically pure L-amino
 726 acids from D,L-formyl- and D,L-carbamoyl-amino acids. Enzyme assays were
 727 performed in triplicate as described in Material and Methods.

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768 **Figure 9.** Profile of L-homophenylalanine production from 100 mM *N*-formyl-
 769 homophenylalanine. L-amino acid at higher concentration of 50 mM is insoluble, but
 770 after 24h of reaction the collected powder is only L-homophenylalanine (data checked
 771 by NMR). Enzyme assays were performed in triplicate as described in Material and
 772 Methods.

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